

# Solubility and Diffusivity Studies

The logo for CSPS (Center for Solubility and Permeability Studies) features the letters 'C', 'S', 'P', and 'S' in a white, bold, sans-serif font with a thin black outline. The letters are arranged horizontally. A large, thick, brown circular arc is positioned behind the 'S' and 'P' characters. A thick, brown diagonal line passes through the 'C' and 'S' characters, extending from the bottom left towards the top right. The background of the logo is a light beige color.

C S P S

# Research Objectives

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**Develop methods to measure phase equilibrium and diffusivity in industrially important polymer-solvent systems**

**Develop models to correlate and predict these properties**



# Applications

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- Drying of films and coatings
- Polymer synthesis
- Devolatilization
- Foam production
- Supercritical extraction



# Experimental Methods

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## Low pressure

- Gravimetric sorption
  - Quartz spring
- IGC
  - Capillary column
  - Packed column
- LLE - HPLC

## High pressure

- Pressure decay
- Capsule
- IGC

# Modeling Efforts

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## Thermodynamics of polymer systems

- Phase equilibria
  - Equations of state – developing a predictive model
  - Activity coefficient models

## Diffusion

- Application of the Vrentas-Duda Free-Volume model
  - Multicomponent

## Processes

- Film dryers – multicomponent solvent, multilayer
- Purge towers (devolatilization)
- Latex polymerization



# Importance of Diffusion

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**Diffusion characteristics are especially important in polymer-solvent systems at high concentrations of polymer.**

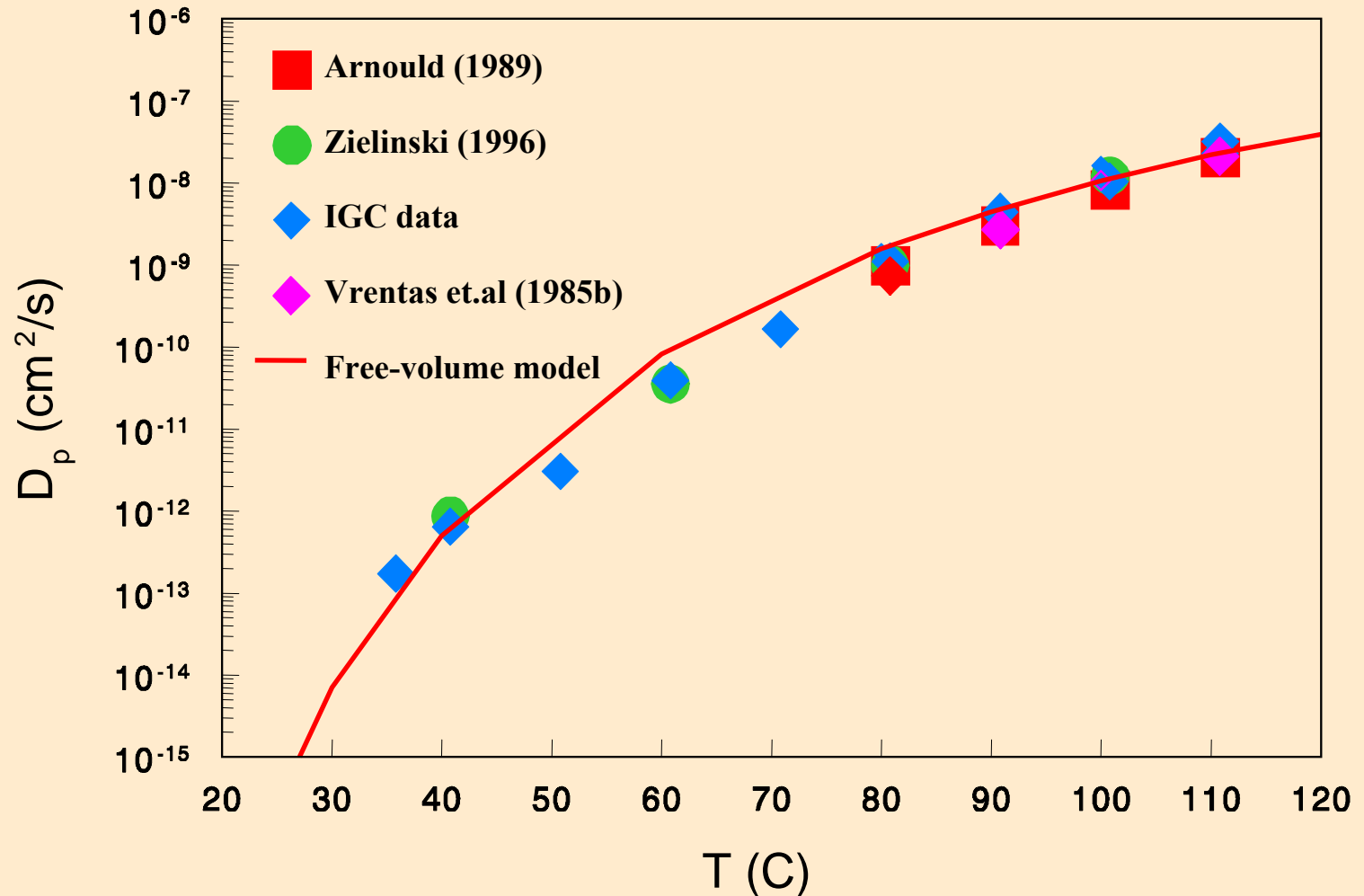
**Strong functions of concentration**

**Strong function of temperature**

**Frequently the controlling factor in the drying or devolatilization process.**



# $D_p$ for Toluene in PVAC



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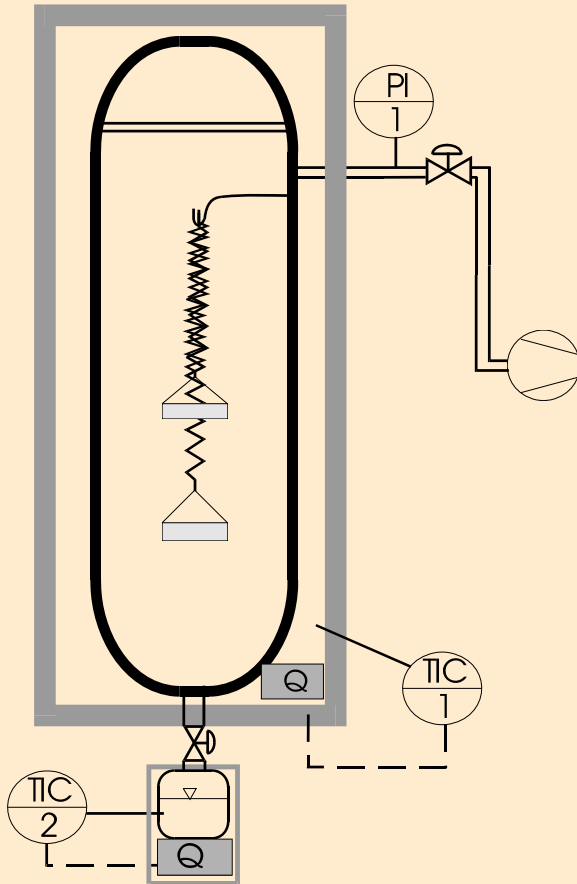
# EXPERIMENTAL METHODS



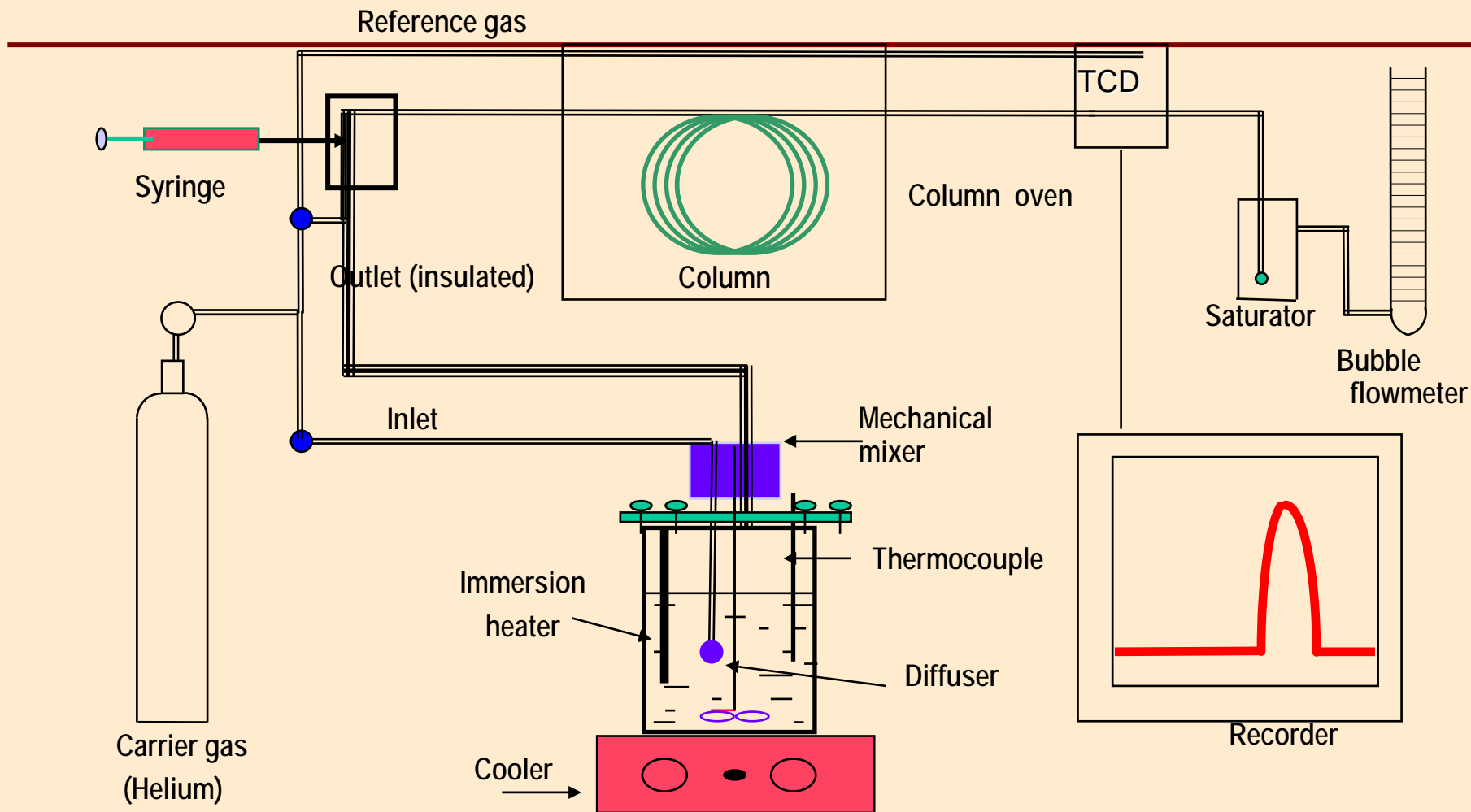
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# Quartz Spring Gravimetric



# IGC Method



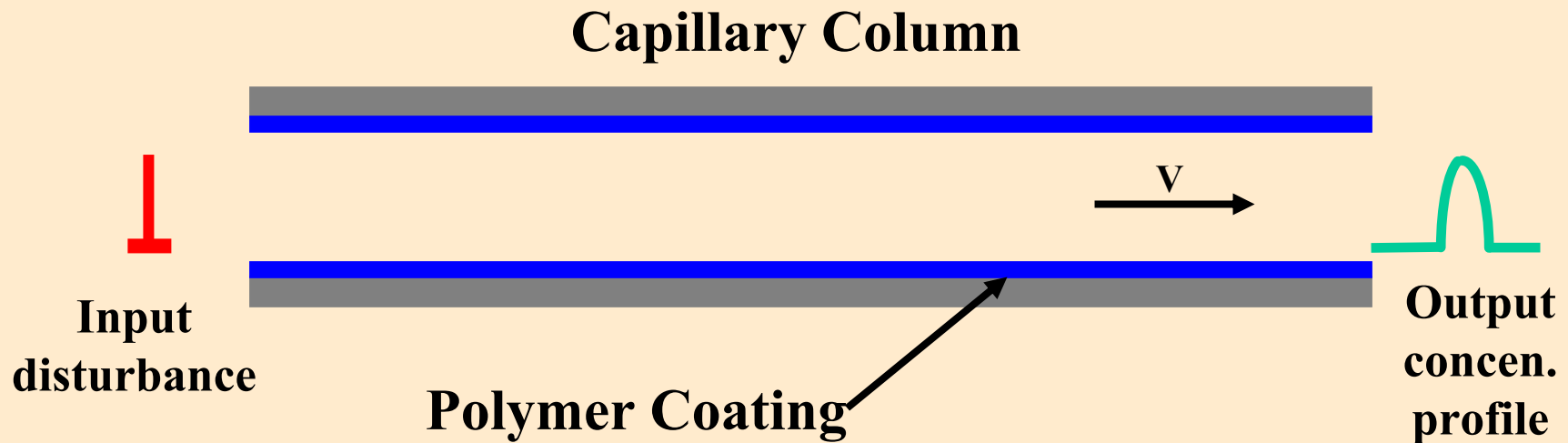
**Finite dilution**



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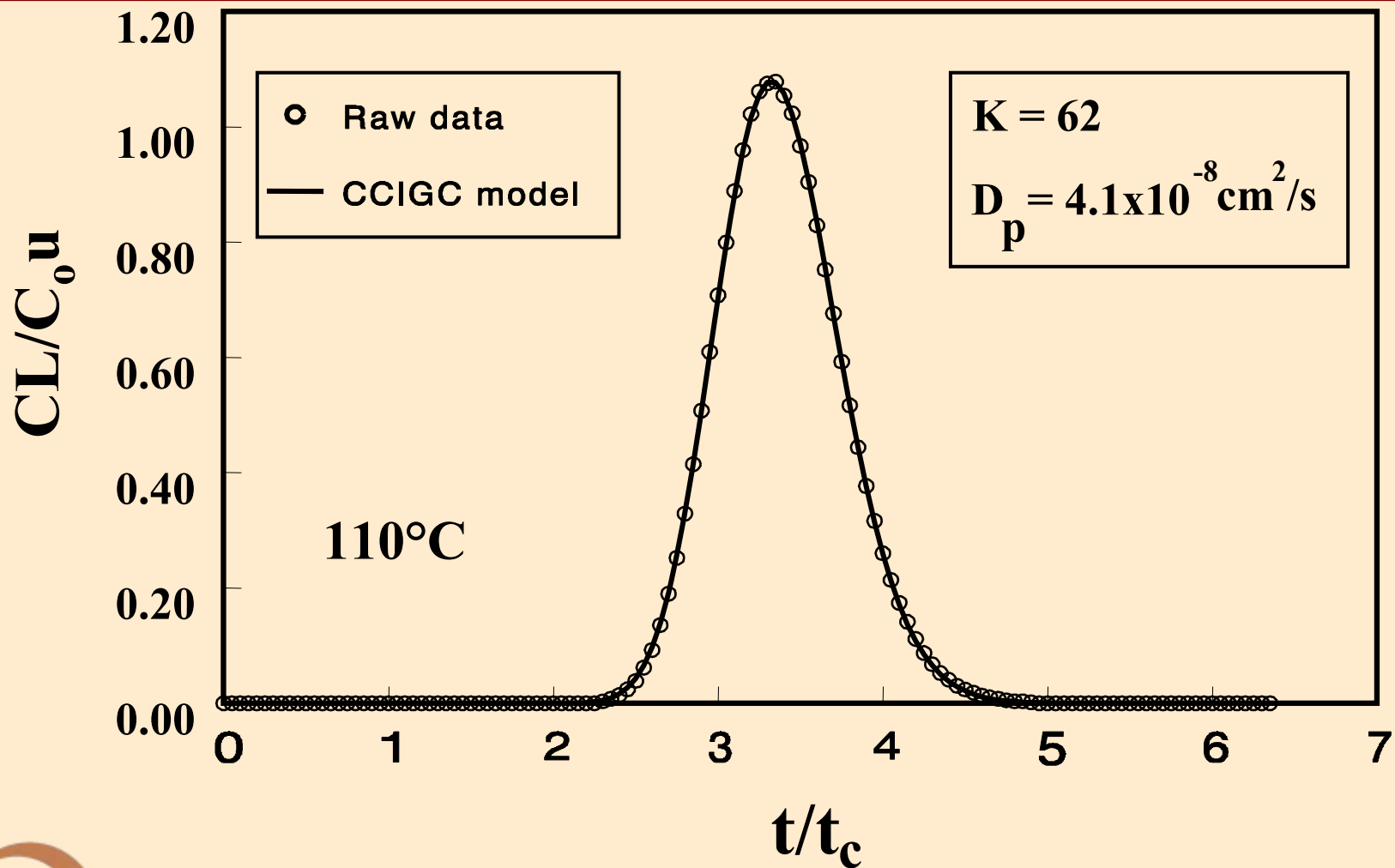
# Inverse Gas Chromatography



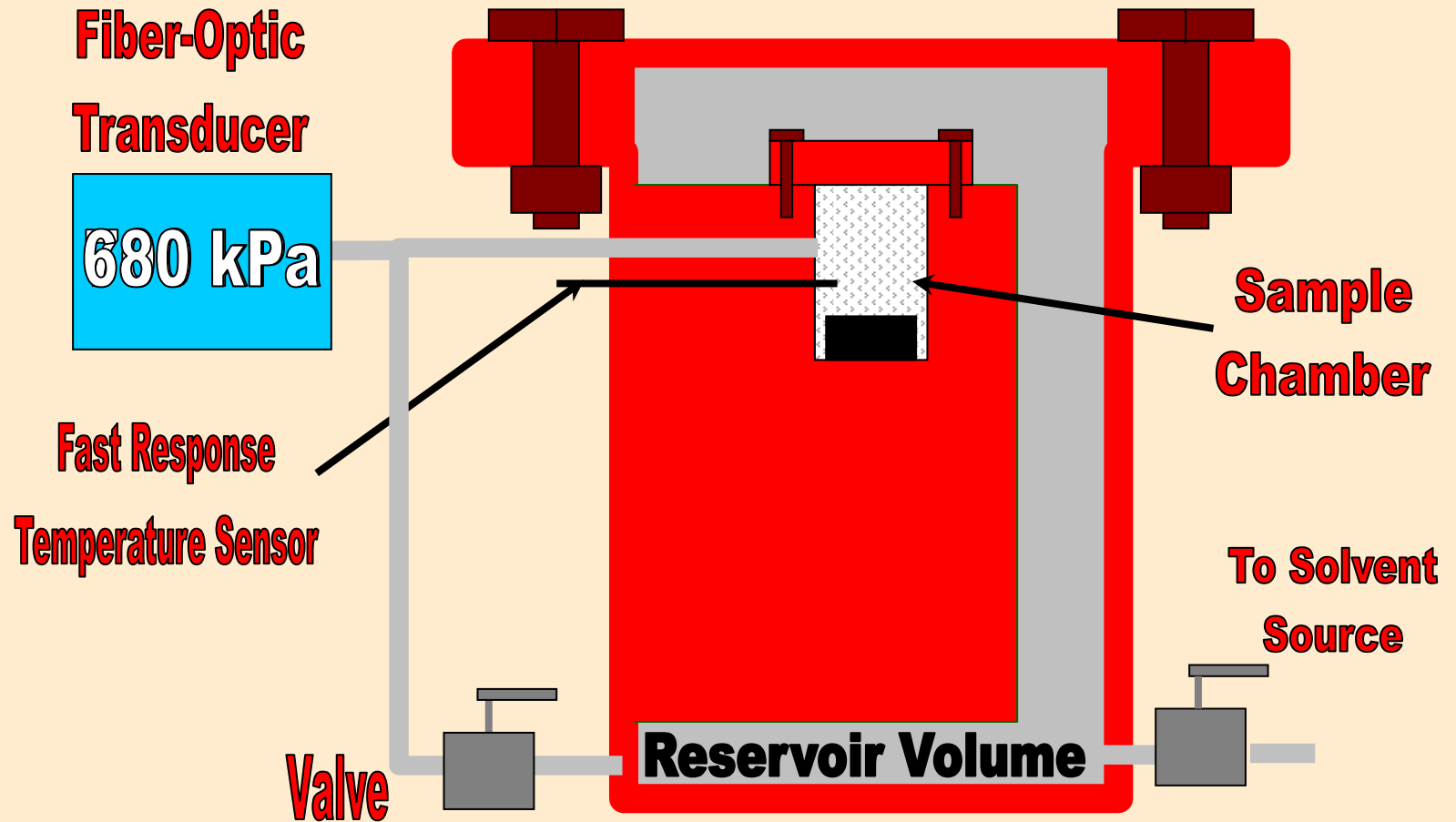
## Contributions to zone broadening

- Longitudinal diffusion in the gas phase
- Mass-transfer resistance in the polymer phase

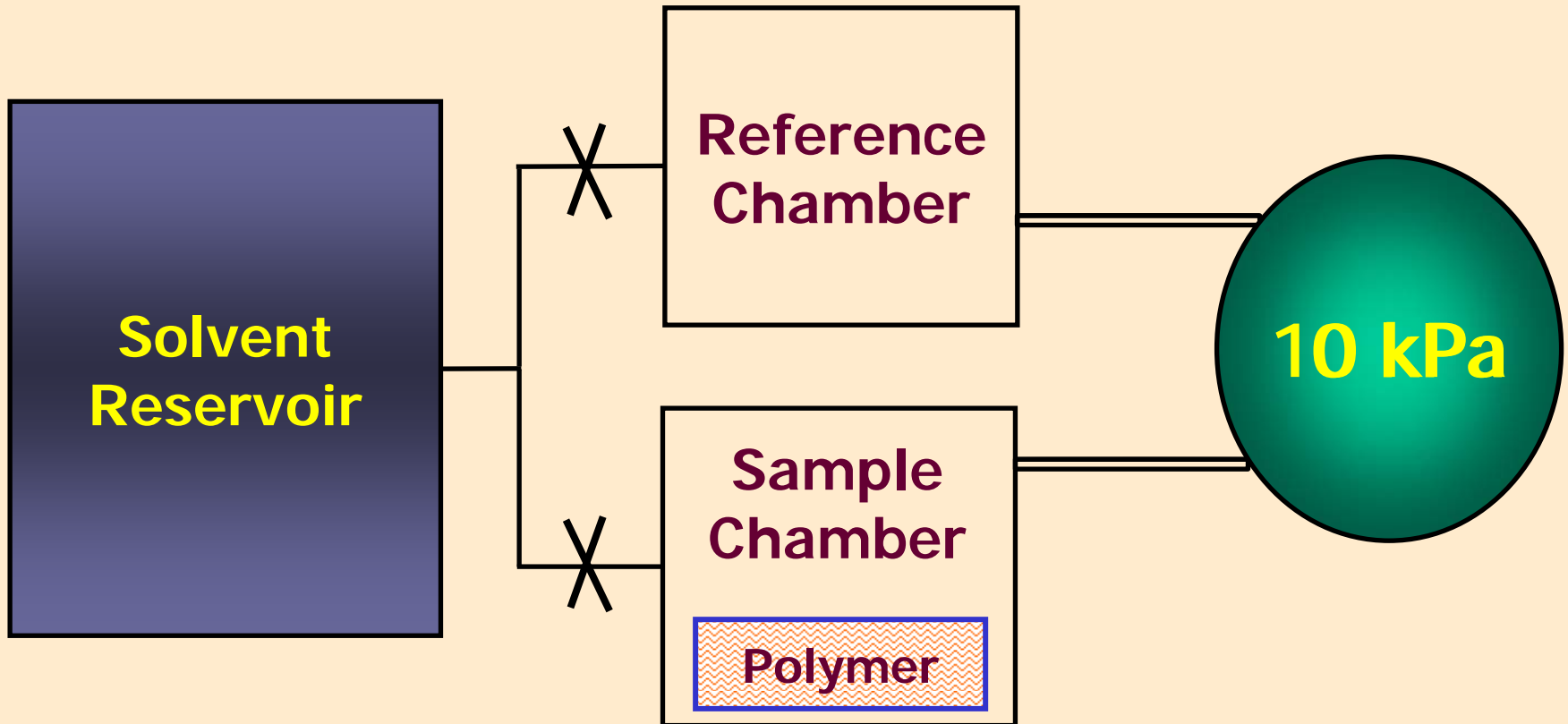
# Elution Profile - Toluene through PVAC



# Pressure Decay Absolute Pressure Apparatus

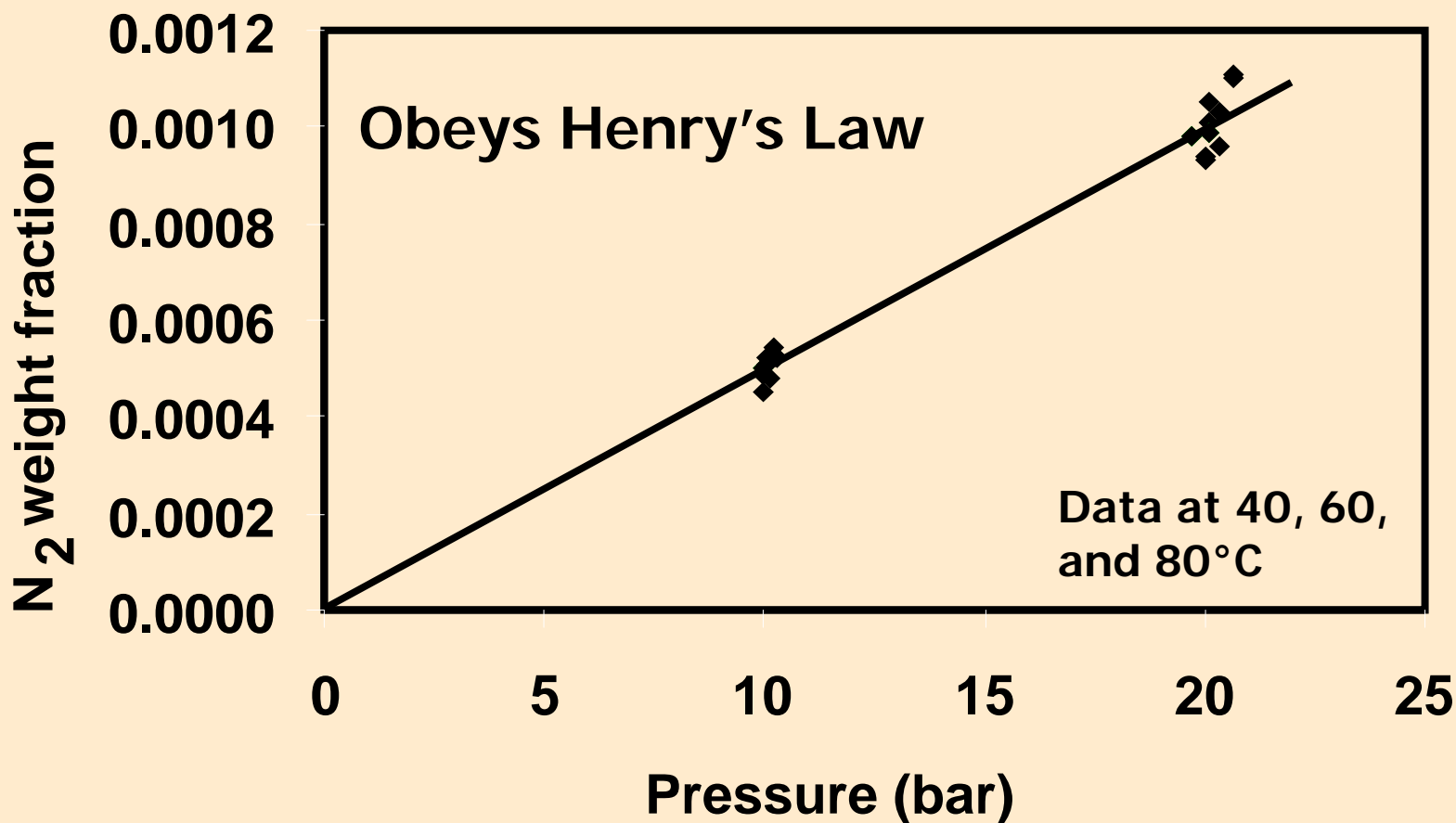


# Pressure Decay Differential Pressure Apparatus

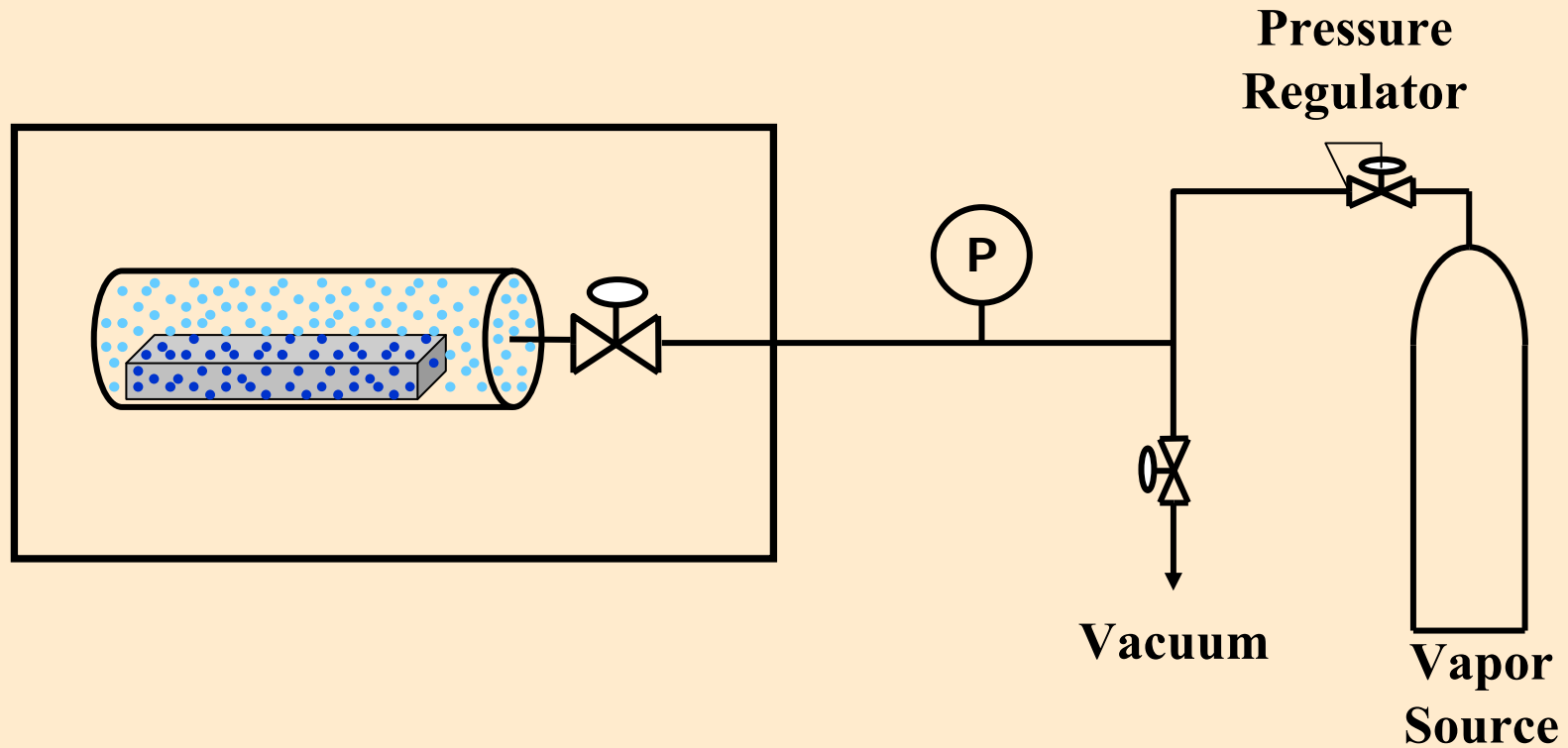


# Pressure Decay

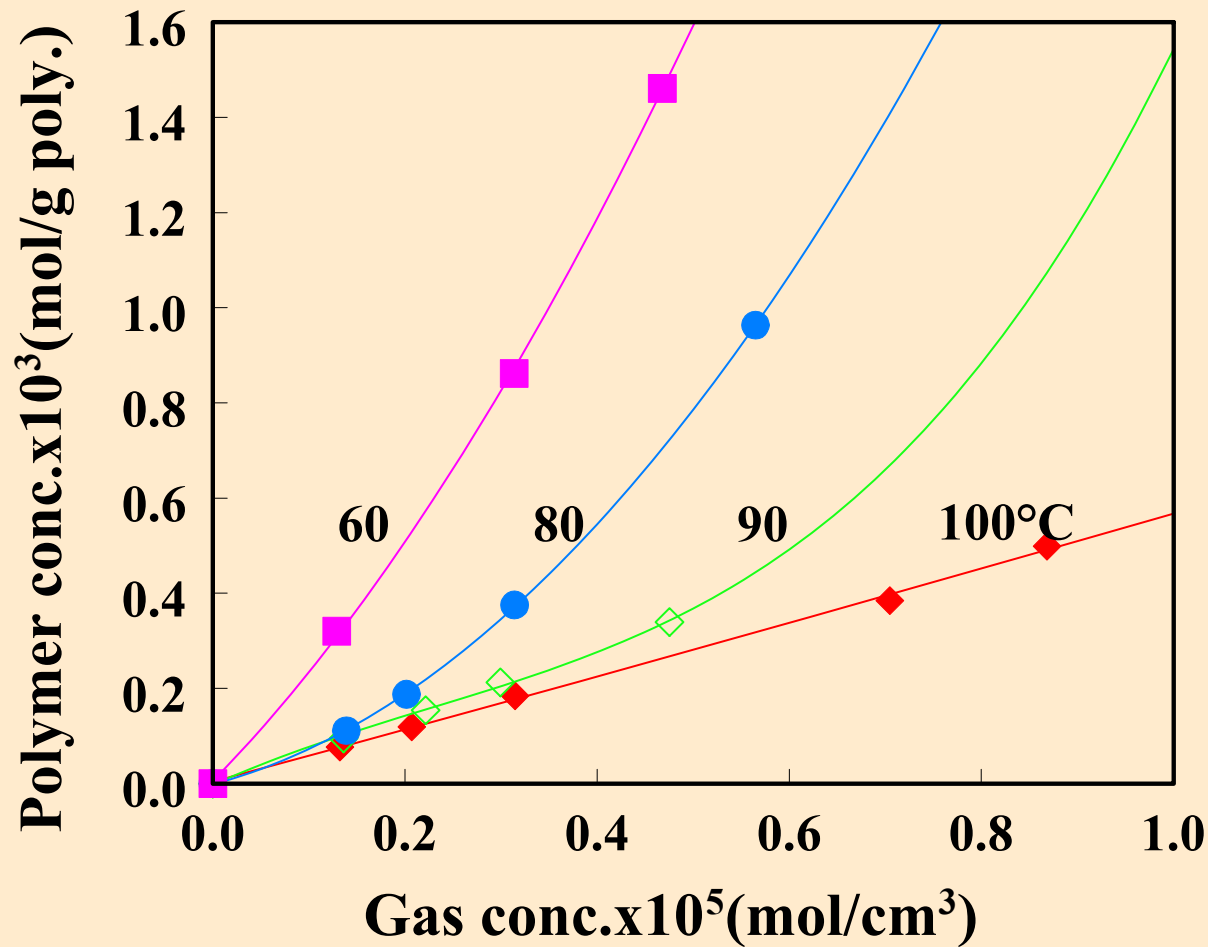
## N<sub>2</sub> Solubility in PVB



# Capsule Method



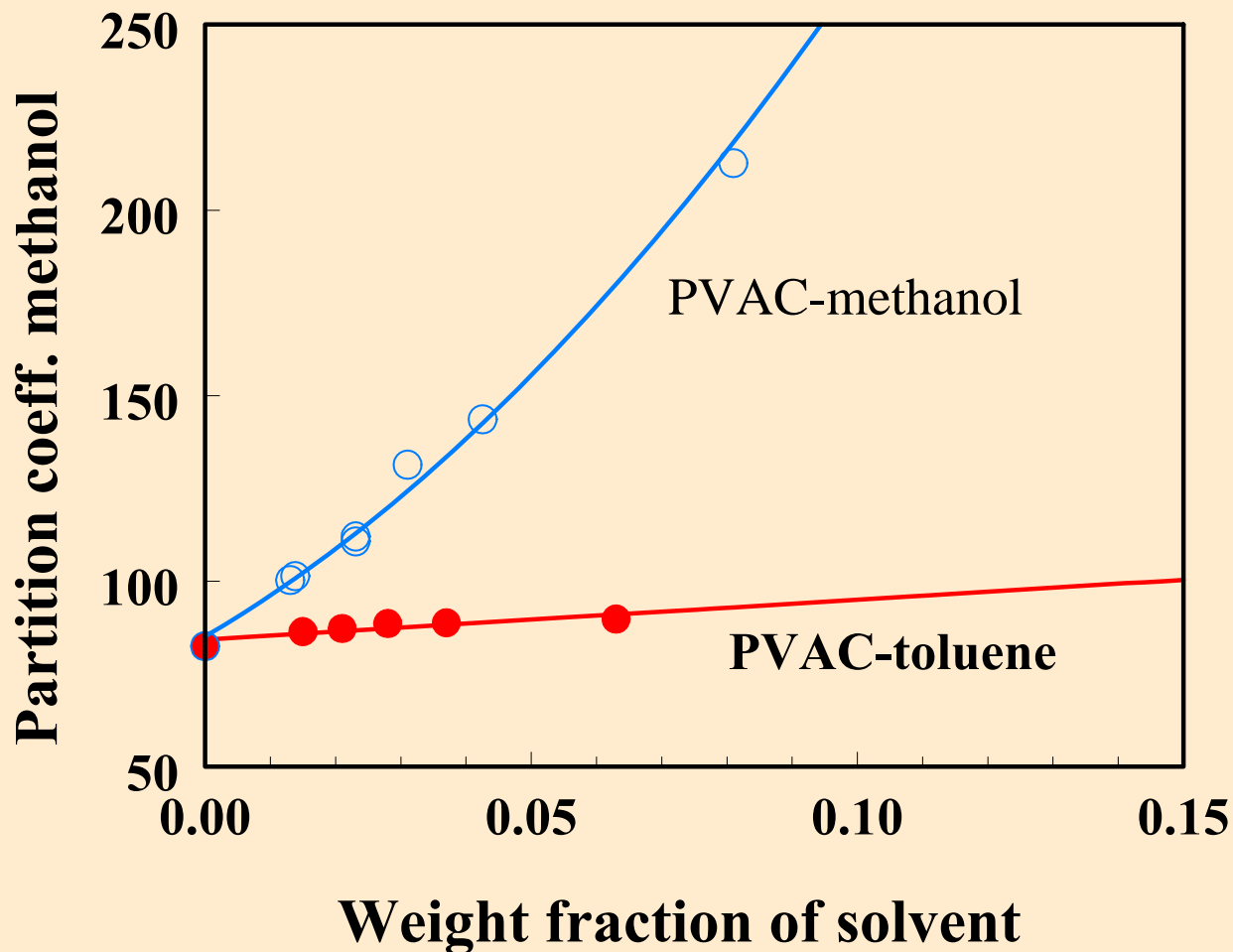
# Sorption Isotherms for Toluene in PVAC



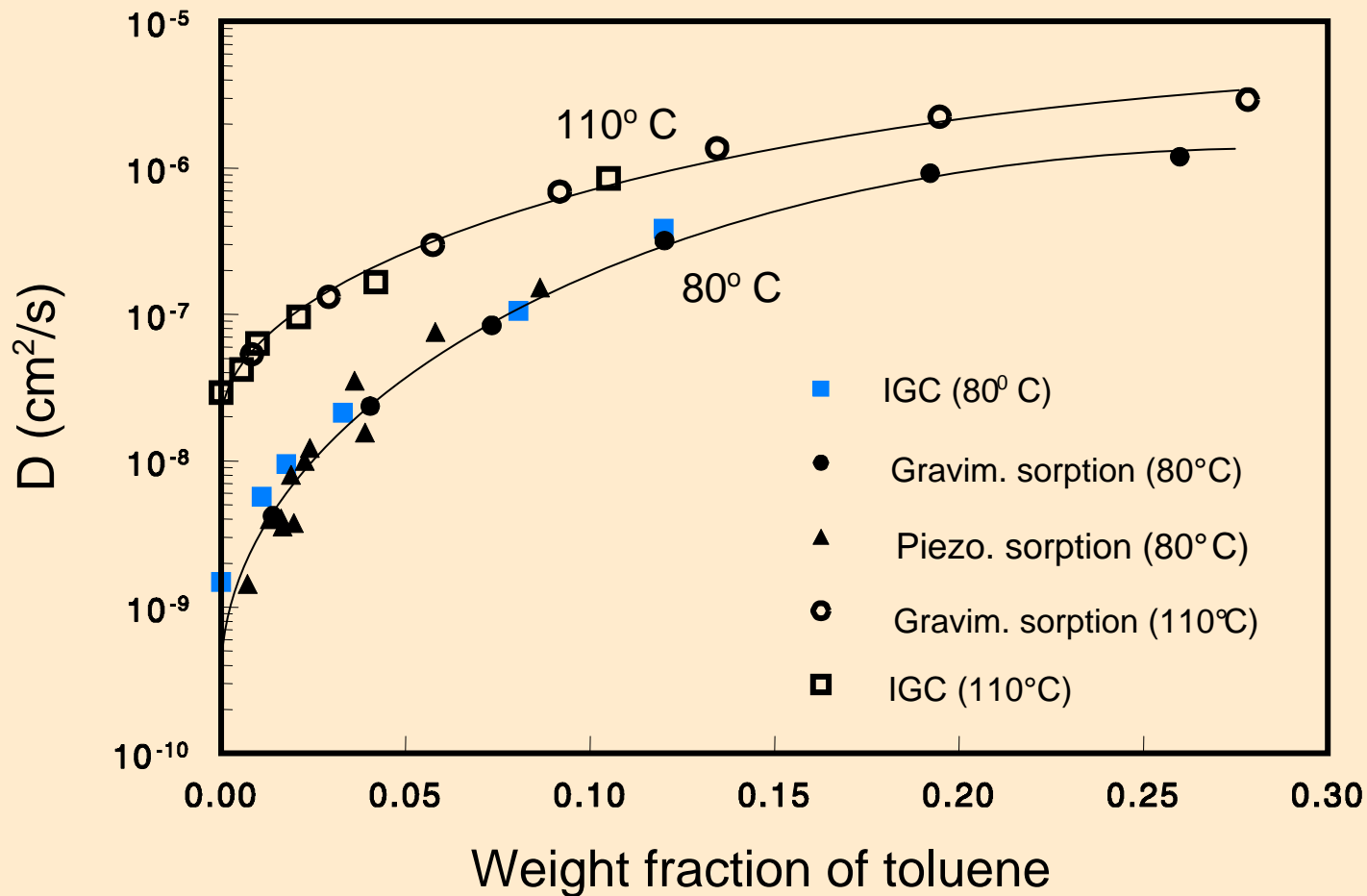
# Partition Coefficient of Methanol in PVAC-Toluene and PVAC- Methanol at 60°C

Partition Coefficient

$$= \frac{\text{conc. polym.}}{\text{conc. gas}}$$



# Comparison of Methods: Toluene in PVAC at Finite Concentrations




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# MODELING EFFORTS



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# Diffusion

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## Vrentas-Duda Free-Volume Theory

**Model based on free volume concept to describe molecular diffusion of solvents in polymers.**

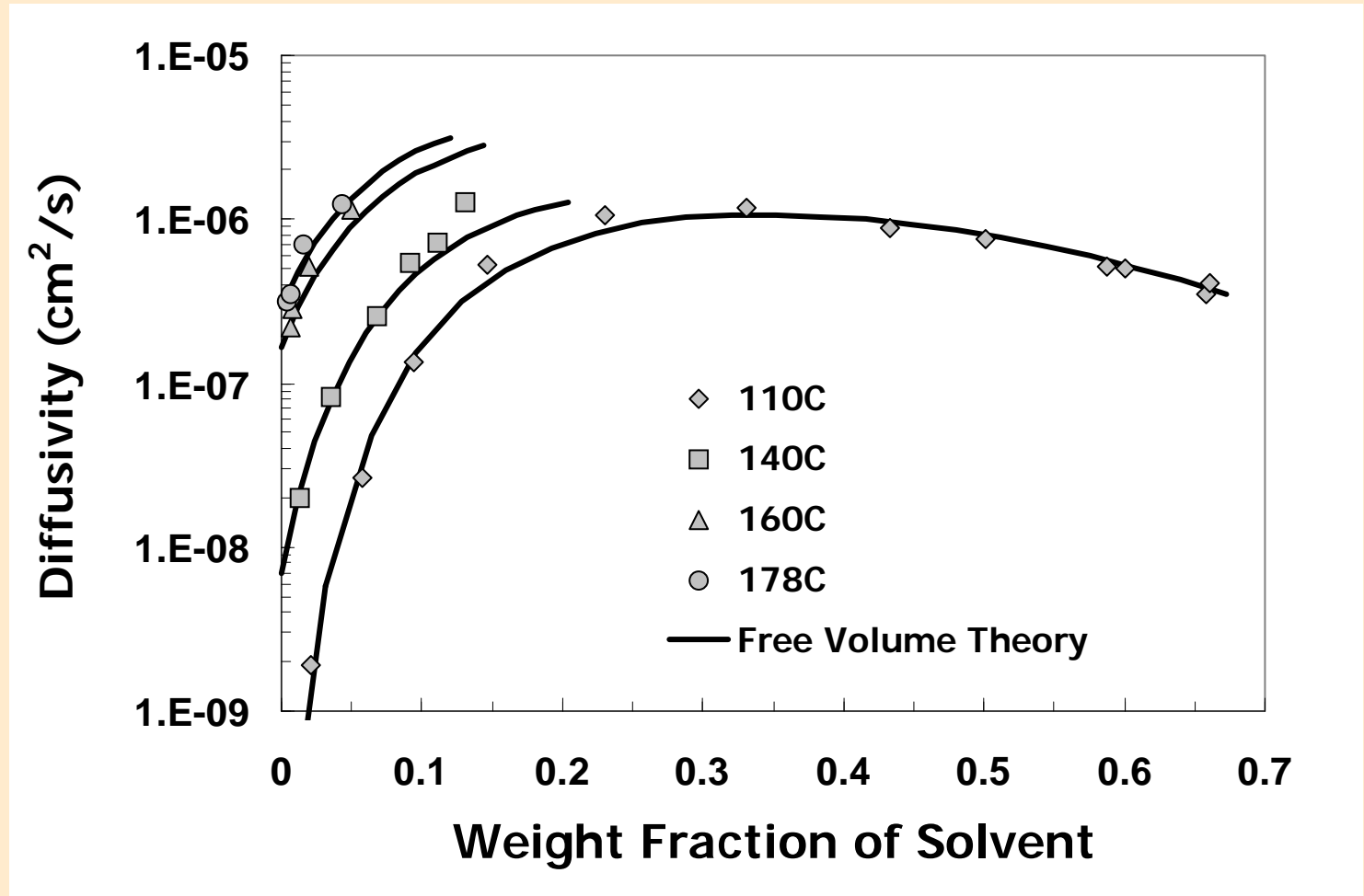
**Necessary events for molecular transport:**

**Hole of sufficient size next to the molecule**

**Molecule possesses enough energy to jump**



# Polystyrene-Toluene



# Implications of Free-Volume Theory

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**Addition of solvent or a temperature increase will increase  $D$  more strongly close to the  $T_g$**

**Larger molecules increase the  $T$  and concentration dependence of  $D$ .**

**Elastomers far above their  $T_g$  have large fraction of hole free volume - large  $D$  with weak  $T$  and concentration dependence.**

**In region of high polymer concentration,  $D$  is very weak function of the molecular weight.**

**Addition of additives effect  $D$  according to their free-volume contribution**



# Phase Equilibria

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## UNIFAC-vdw-Free Volume

Activity coefficient approach (low pressure)

Group-Contribution, Lattice-Fluid EoS  
Equation of state approach

SAFT EoS



# UNIFAC - FV

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WFAC of a solvent in the polymer,  $\Omega_i$ , is given by:

$$\ln \Omega_i = \ln \Omega_i^C + \ln \Omega_i^R + \ln \Omega_i^{FV}$$

# GCLF-EoS

## Panayiotou-Vera EOS

$$\frac{\tilde{P}}{\tilde{T}} = \ln\left(\frac{\tilde{v}}{\tilde{v}-1}\right) + \frac{z}{2} \ln\left(\frac{\tilde{v} + q/r - 1}{\tilde{v}}\right) - \frac{\theta^2}{\tilde{T}}$$

$\tilde{P}$ ,  $\tilde{T}$  and  $\tilde{v}$  are reduced quantities expressed as :

$$\tilde{P} = P/P^* \quad \text{where} \quad P^* = z\varepsilon_{11}/2v_h$$

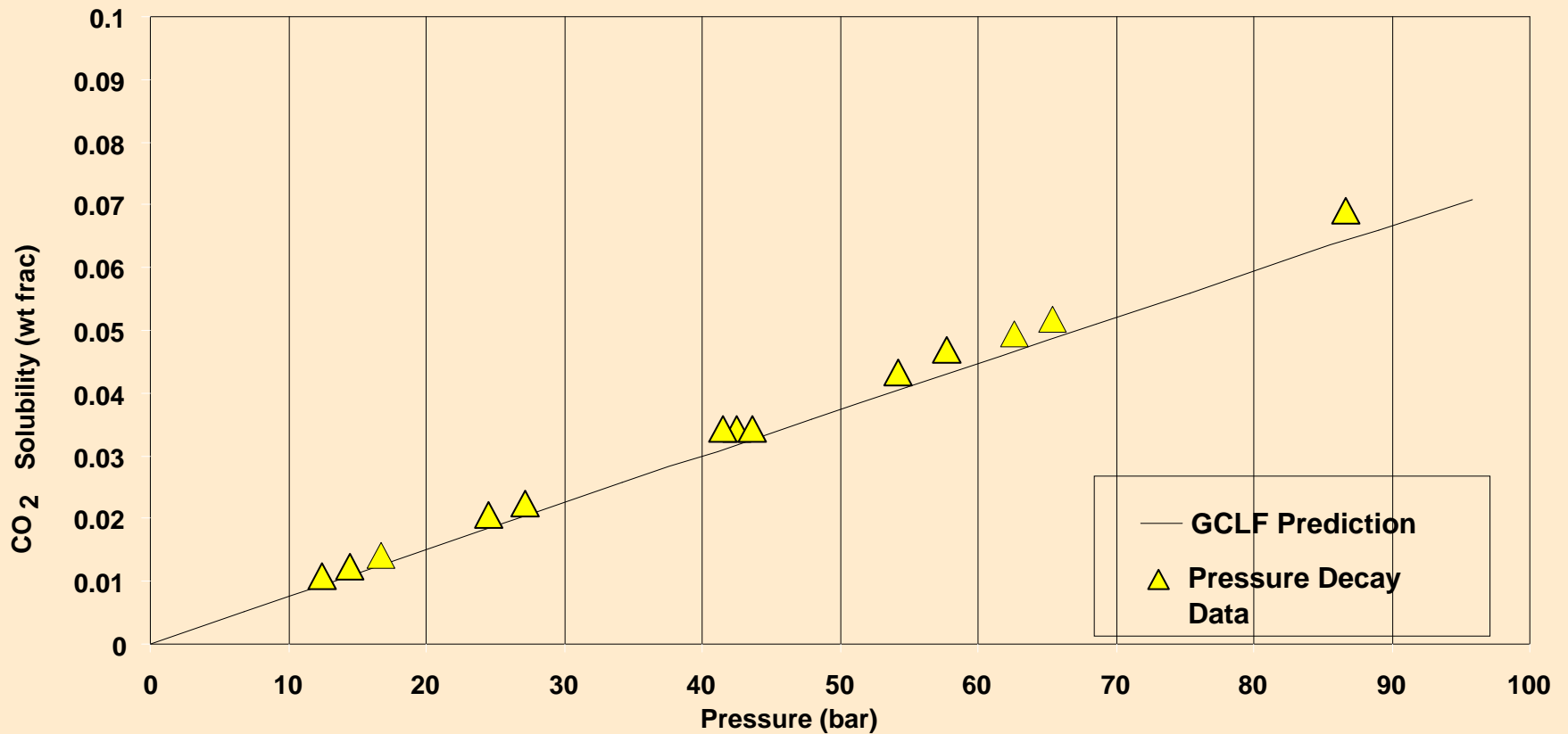
$$\tilde{T} = T/T^* \quad \text{where} \quad T^* = z\varepsilon_{11}/2R \quad \tilde{v} = v/v^*$$

Two scaling parameters per pure component:  $v^*$  and  $\varepsilon_{11}$

and an interaction parameter,  $k_{ij}$ , for mixtures. These parameters are obtained using the group contributions methods developed by Lee and Danner.

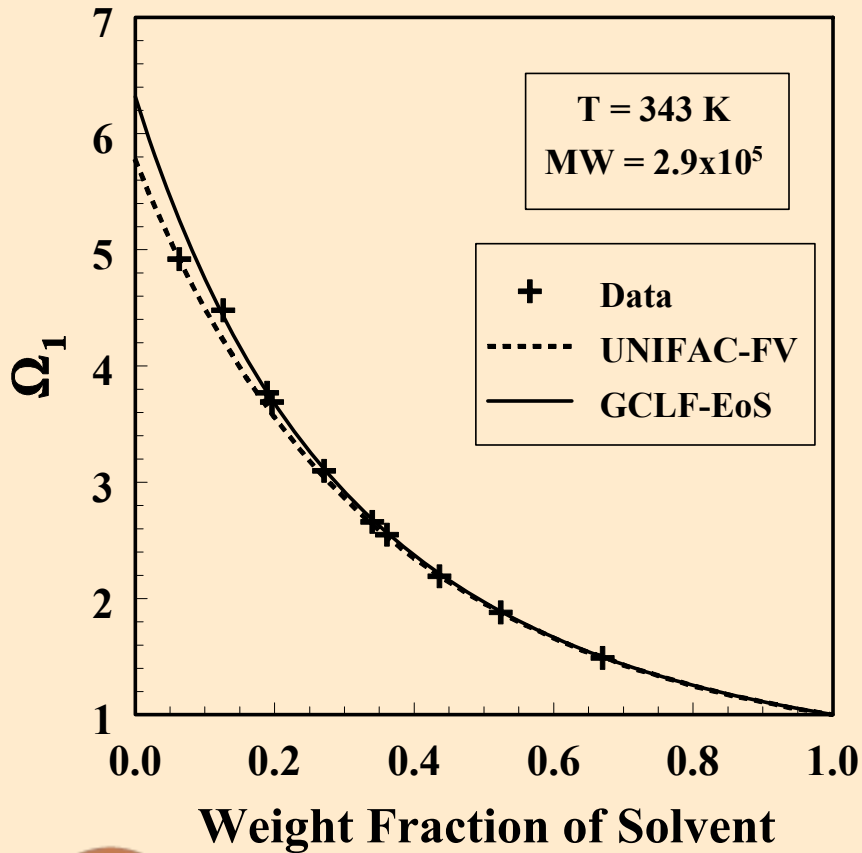
# GLCF-EoS

## CO<sub>2</sub> – PP at 170°C

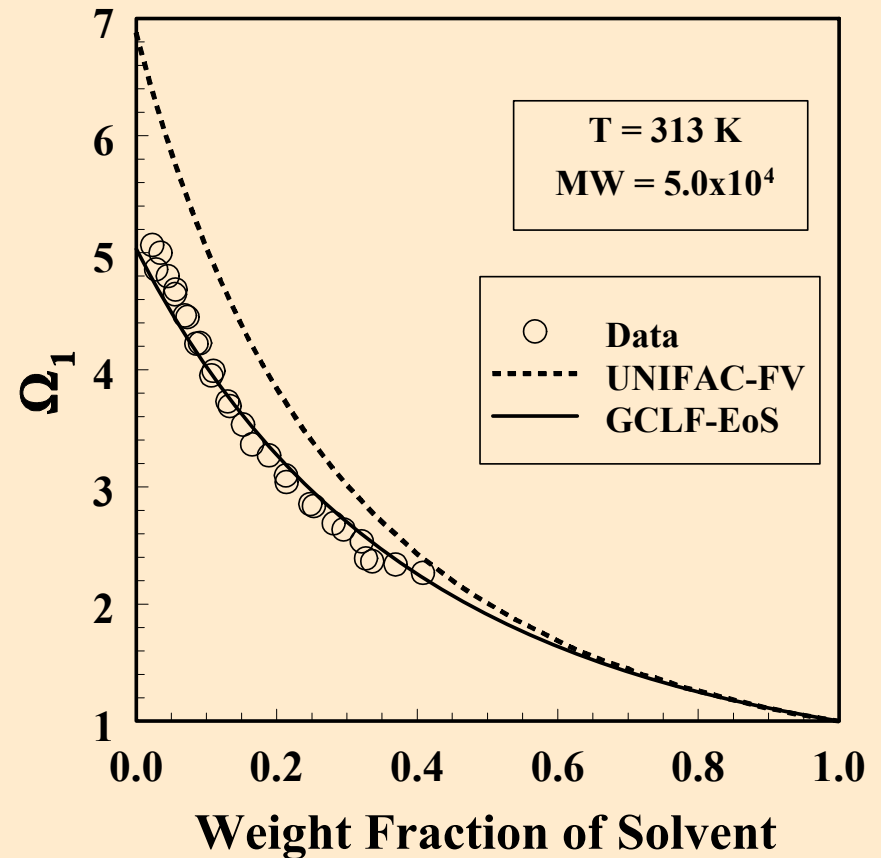


# GCLF-EoS – UNIFAC-FV

## PS/n-Propyl Acetate



## PIB/Benzene



# Conclusions

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**Extensive capabilities to measure and model:**

**Phase equilibria in polymer-solvent systems –  
primarily VLE**

**Mass transport in polymer-solvent systems**

**Wide application in polymer processing and  
production.**

